



Experience gained from the former ore processing and the remediation of the site.

M. Csővári, G. Földing, Zs. Berta, G. Németh

MECSEK-ÖKO Zrt, Pécs, Hungary

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PRESENTATION OUTLINE

- 1 Summary of the remediation works
- 2 Lessons and experience gained from the former mill process
- 3 Lessons and experience learned from the remediation



DECREASING OF THE RADIOLOGICAL IMPACT

1 <u>To decrease</u> the radiological impacts to the exceptable level, and long-term stabilization of the radiologically contaminated wastes

This goal is fully achieved

- •Shafts are backfilled, waste rock piles are landscaped, and covered
- •Mill and other facilities are demolished or cleaned-up, yards, industrial roads are cleaned-up, heap leaching residues have been relocated, sites have been remediated
- •Tailings ponds are stabilised, and covered

Altogether the radiological parameters (γ-dose rate, radon exhalation, etc) on the sites ARE IN COMLIENCE WITH all requirements, limits established by the authorities.



GROUNDWATER PROTECTION

2 Restoration and protection of the groundwater and surface water quality from contaminants.

This work is being underway in accordance with the original plans

In this respect:

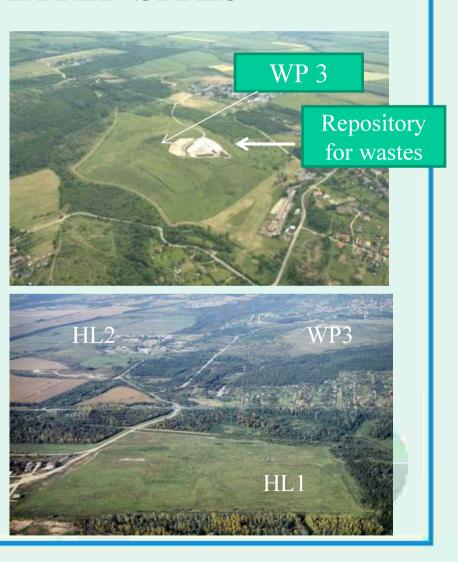
- Groundwater restoration system and water treatment station have been built: app. 0.5 million m³/a of contaminated water is being extracted in the vicinity of the tailings ponds and treated. App. 44 kt of solute (TDS) has been removed by this way.
- •Water treatment station was built for the uranium-contaminated mine water and seepage from waste rock piles
- •In-place uranium treatment columns are in operation in some places
- •Experimental permeable reactive barrier has been istalled for in situ groundwater treatment

1 Summary of the remediation work



SOME REMEDIATED SITES







GROUNDWATER RESTORATION AND WATER TREATMENT STATIONS





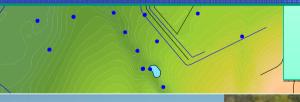
•Extraction wells: 27

•Horizontal

drain: 3.3

For the remediation app. 83 million Euro was spent s For long-term monitoring and water treatment app. 2.5 million Euro is needed yearly





m³ /a is being extracted



Groundwater restoration

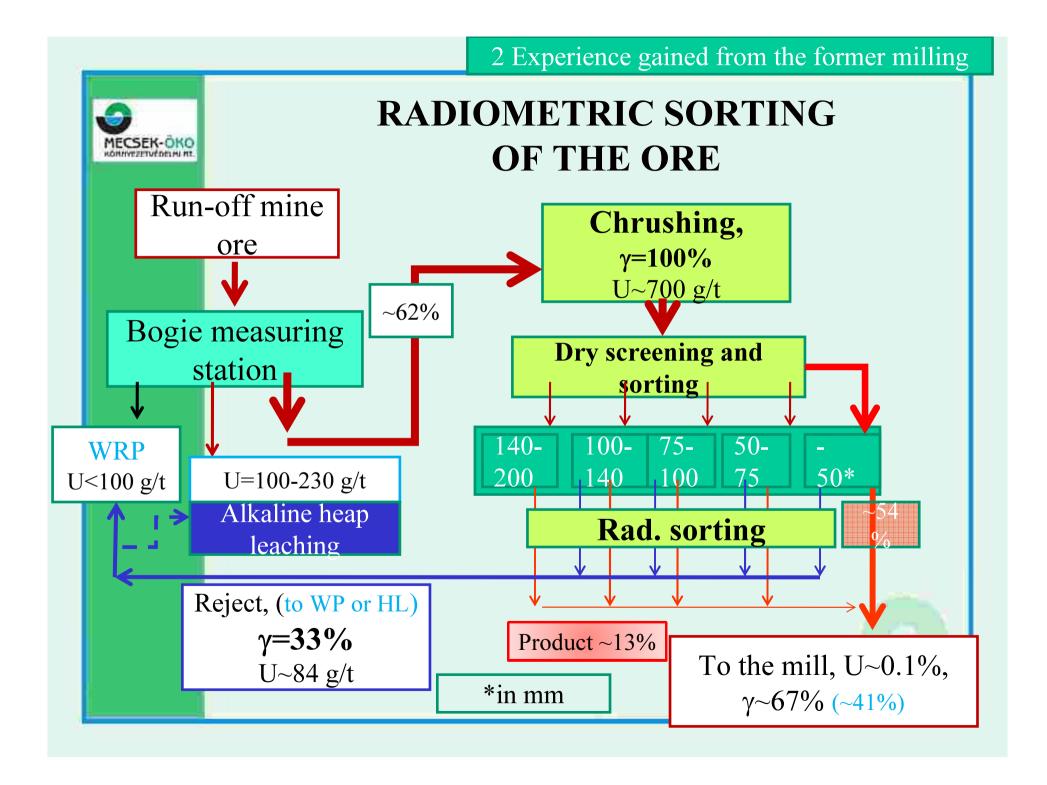


2 Experience from the former milling

Flow sheet:

Conventional acid leaching (18.5 Mt) and alkaline heap leaching (7.2 Mt) for low-grade ore

- 1 Radiometric sorting
- 2 Leaching
- 3 Regeneration of the hydrochloric acid used for the eluation





ACID LEACHING

The leaching process was continuously developed

because the (branerite)

Only small part (~12%) of the ore is leached at low free acid concentration

Pulp from

thickener

Main milestones of the development:

One stage leaching

Separate leaching of the sand-fine

with dividing the pulp into four portion by hydrociclones and adding the bulk of acid into the first stage

Hydrociklones

Free acid

 \sim 5 g/l

For: sandy part~ 60-30 g/l Fines~10-15 g/l

150 _______ 12 g/l

U recovery

 $\sim 89\%$

~92%

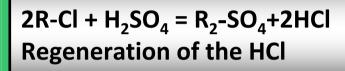
Acid

~94%

To the milling



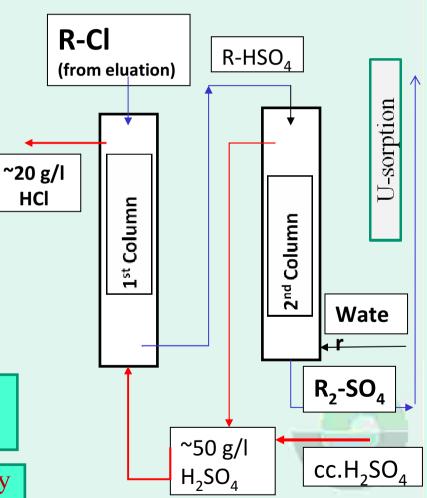
REGENERATION OF THE HYDROCHLORIC ACID FOR ELUATION



 $R-CI + HSO_4^- = R-HSO_4 + HCI$ Washing $R-HSO_4 \longrightarrow R_2-SO_4$ $+H_2SO_4$ $2^{nd} Column$

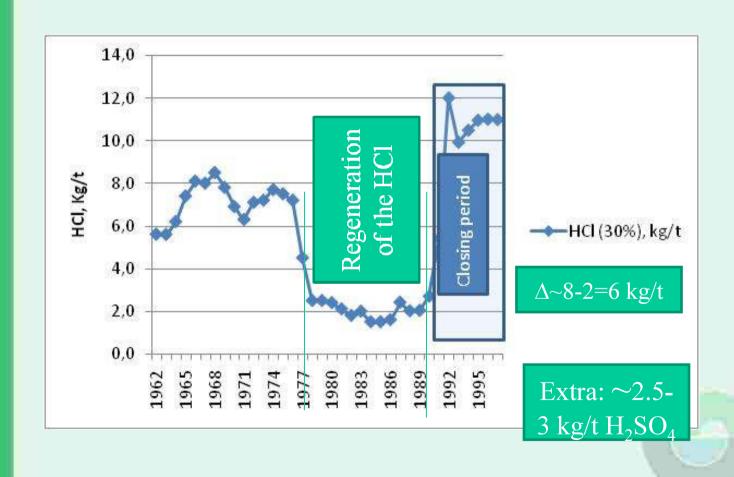
Spec. consumption: 1.4 kgH₂SO₄/kg HCl

Decreasing of the chloride consumption by ~2 kg/t



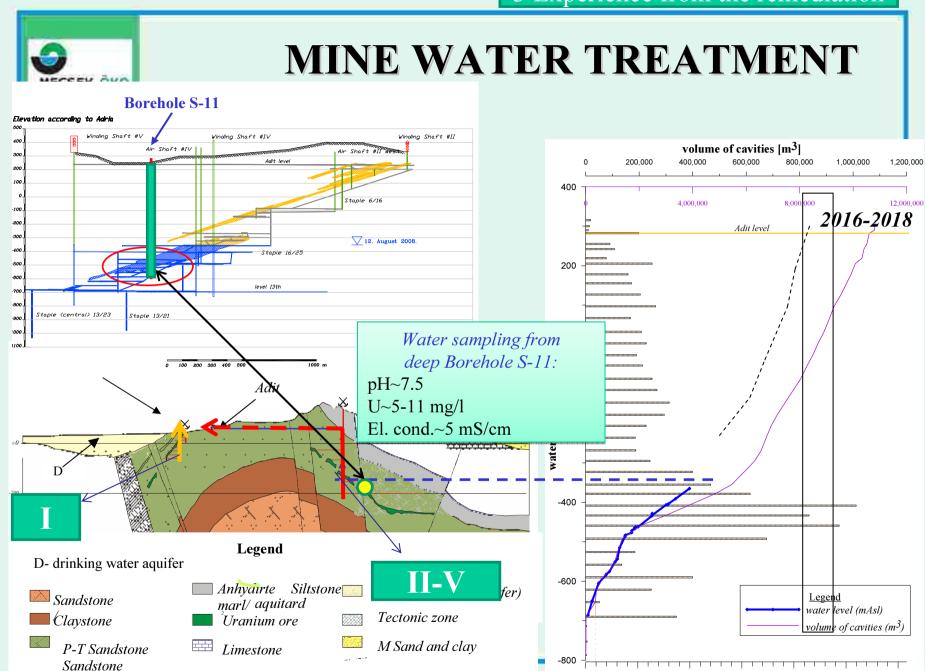


DECREASING OF THE CONSUMPTION OF THE HCI FOR ELUATION





- 3.1 Mine water treatment
- 3.2 Heap leaching
- 3.3 Groundwater contamination and restoration on TPs area
- 3.4 TPs remediation
- 3.5 Passive/semi-passive methods of water treatment



1999-

08-28

2003-

08-27

2007-

08-26

2015-

08-24

2011-

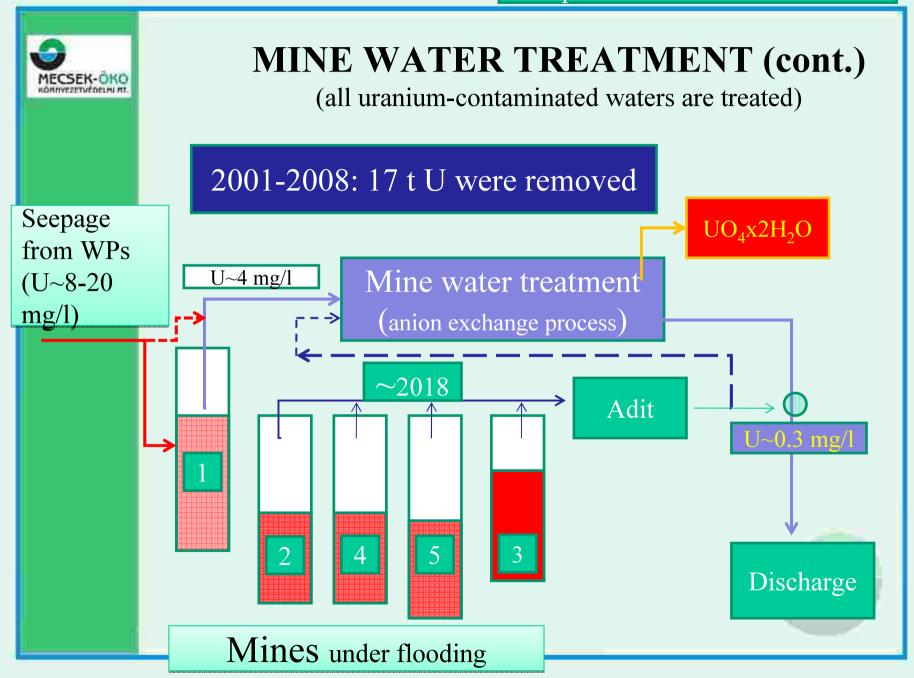
08-25

2023-

08-22

2019-

08-23





HEAP LEACHING RELOCATION OF RESIDUES TO THE FINAL STORAGE AREA

Site II

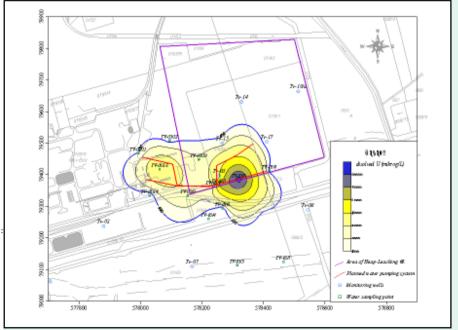




GW CONTAMINATION ON HL-SITES



Contamination was observed first of all nearby the pumping stations and pipe lines





HEAP LEACHING PRACTICE



7.2 million t low grade ore was treated (~140 g/t), ~60% recovery (540tU), 5kg/t Na₂CO₃, 37 ha

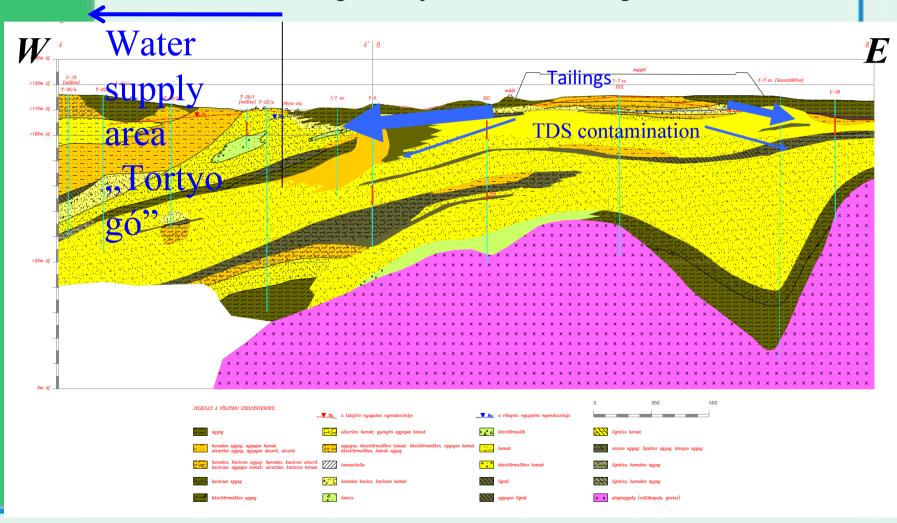
How to improve the process?

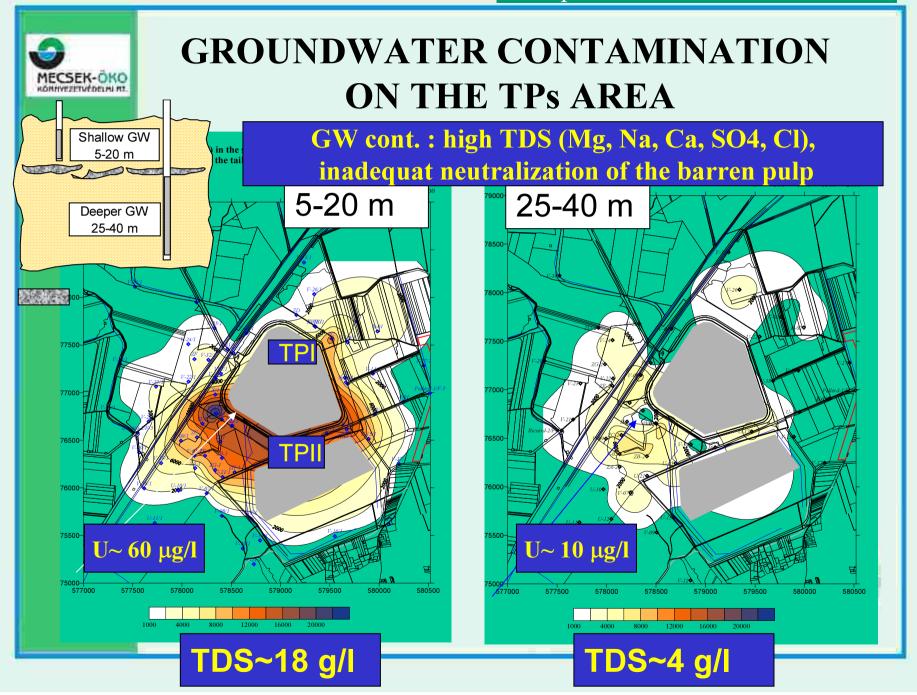
Continuously expanding pads need rather large area (in our case 6.5 ha/Mt). Therefore reusable pads seem to be more reasonable with the disposal of the residues on the final storage area.

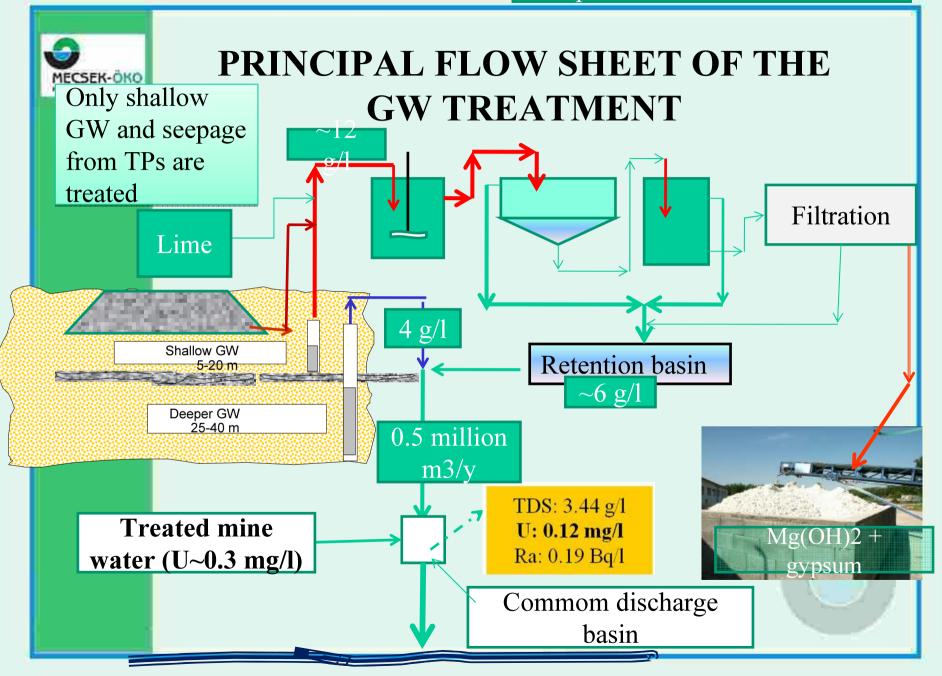


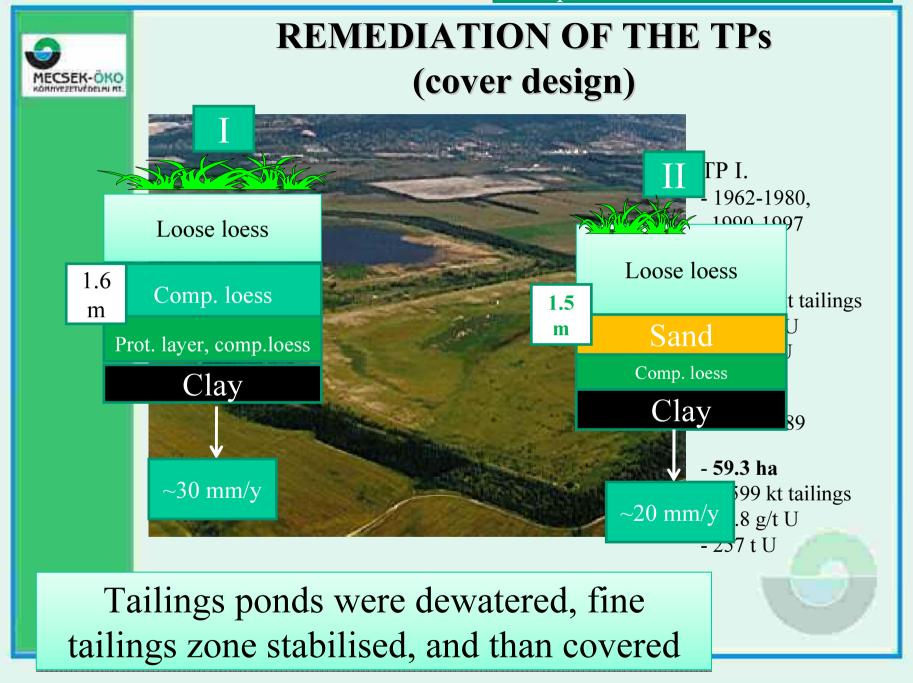
HIDROGEOLOGICAL SITUATION AROUND THE TPs

Geological Profile across the Tailings Pond



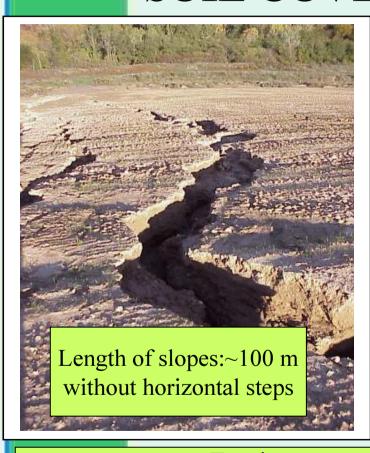








WATER EROSION OF THE SOIL COVER ON TAILINGS PONDS





Erosion was reduced by making furrow ditches to divert the water flow



STABILIZATION OF THE FINE TAILINGS ZONE



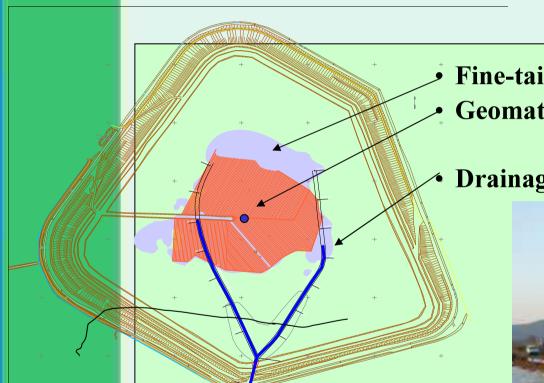
Special task
was the
stabilization of
the weak slime
zone

Field test for receiving experience

Cooperation with Wismut and C &E



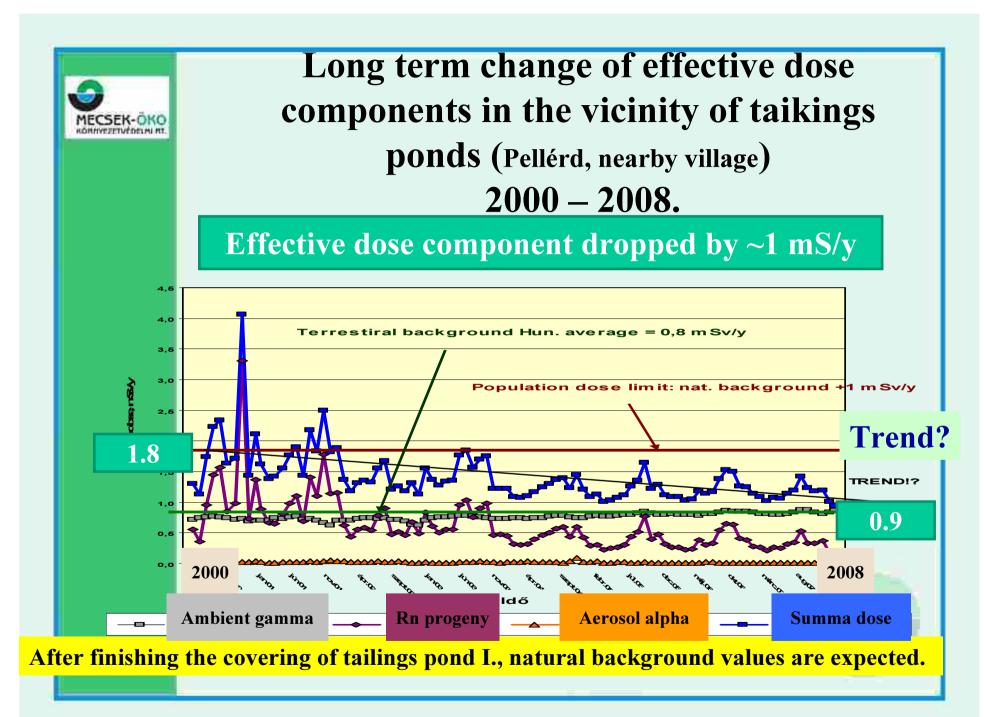
DRAIN IN FINE TAILINGS



- Fine-tailings zone
- Geomaterial (13 ha)
- Drainage trench

Length: 1050 m depth: 4-6 m

d:160 mm Q \sim 40 m³/d (\sim 0.076 m³/m²/d)

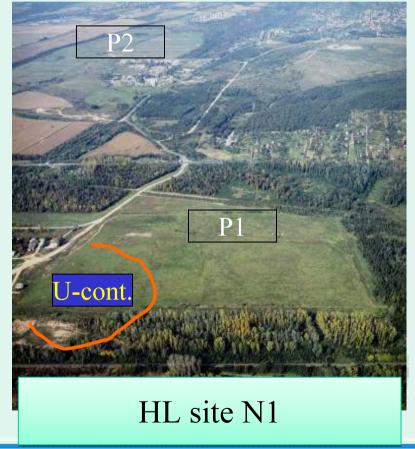




IN-PLACE WATER TREATMENT (on WP and former HL)



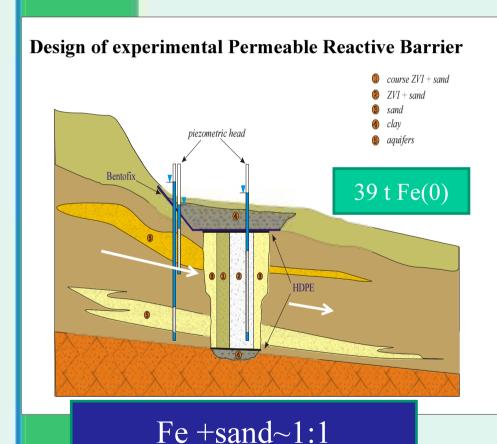
Seepage from WR (Fricitáró, ~40 m³/d)

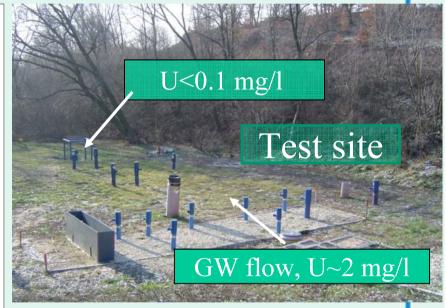


Passive/semi passive methods of water



EXPERIMENTAL PERMEABLE REACTIVE BARRIER (for in situ water treatment)



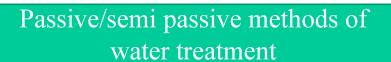


28 monitoring

wells

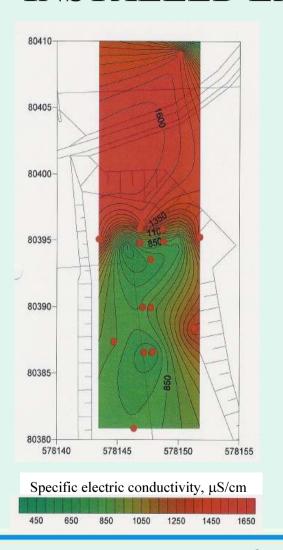
Installed: August 2002

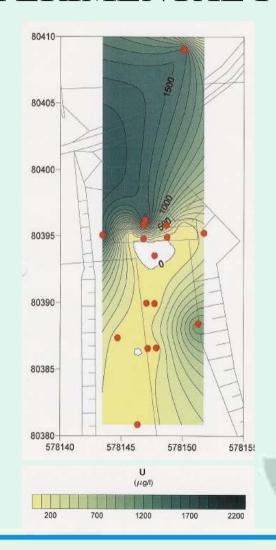
PEREBAR- EU-sponsored project





LONG-TERM PERFORMANCE OF THE INSTALLED EXPERIMENTAL PRB





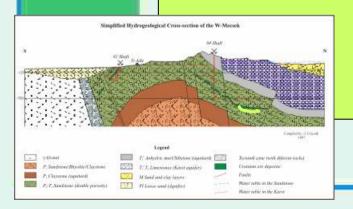






Ore reserves (left behind on the site)

- •Mining and processing of U-ore was terminated in 1997 because of economical reason
- •Total estimated <u>solid</u> ore reserve (U~0.12%):
 - •39 Mt (up to -1300 m depth)
- •From which mined out <u>solid</u> ore was 20 Mt (28 Mt in form of run-off-mine ore)
- •Reserves left behind: 19 Mt



12 Mt (1200-1300 m)

7 Mt (1000-1200 m)

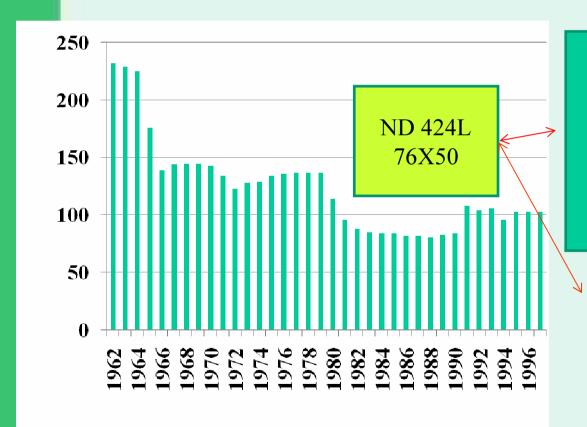


THANK YOU FOR YOUR KIND ATTENTION





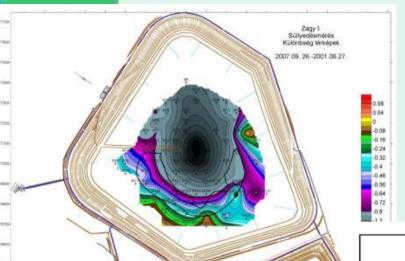
DEVELOPMENT OF THE RADIOMETRIC SORTING PROCESS OF THE ORE



Decreasing the background and installation more sensitive detectors

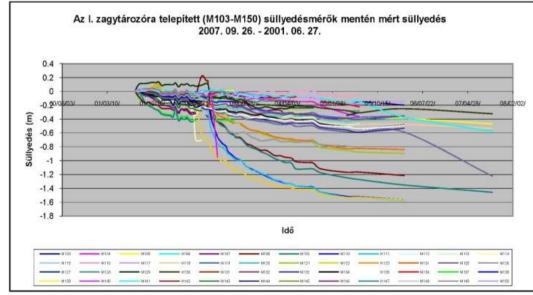
Detection efficiency: 5600 imp/s/gU





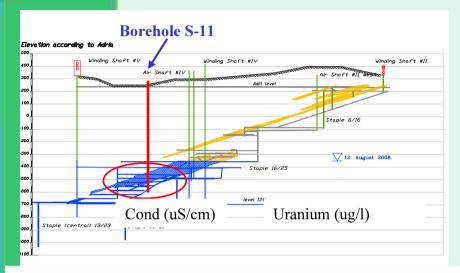
3.4.4 SUBSIDENCE ON THE SLIME ZONE (2001-2007)

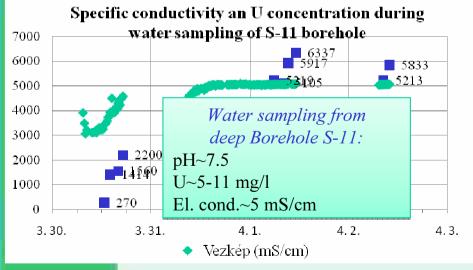
Maximum: 1.6 m/7 years, Presently~2 cm/y

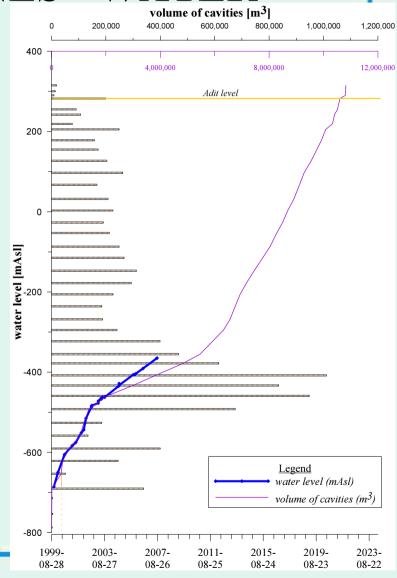




3.1.2 URANIUM CONCENTRATION IN DEEP MINES' WATER

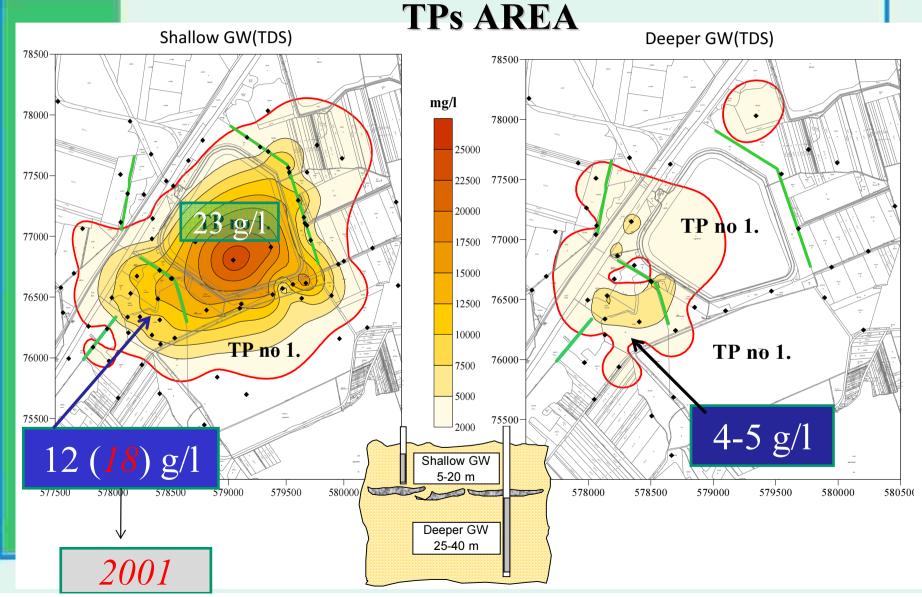








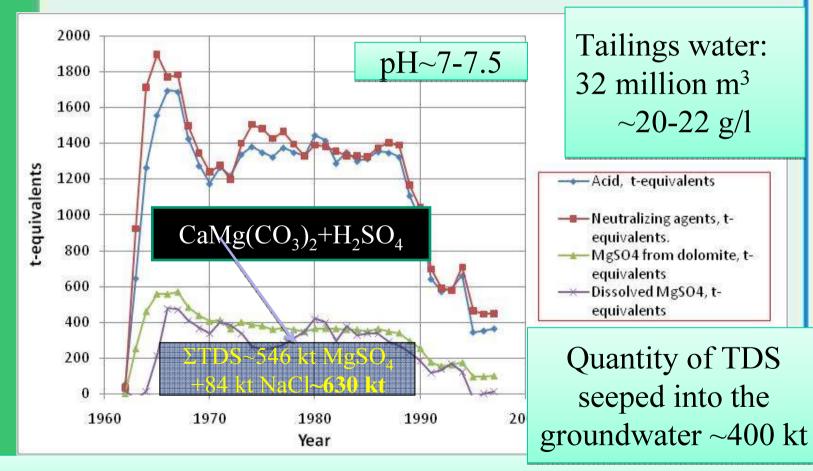
MECSEK-OK 3.4 GROUNDWATER CONTAMINATION ON





2.4 ESTIMATION OF THE TDS IN TAILINGS WATER

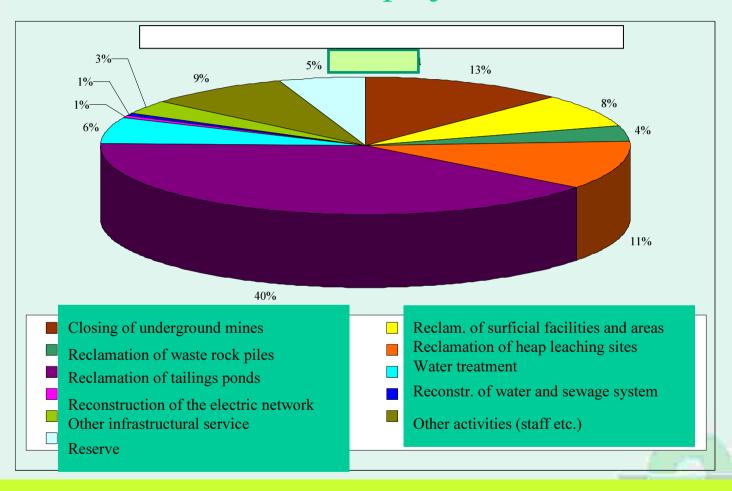
(Balance of acid and neutralizing agents [lime, lime stone grinds, dolomite from the ore] in the mill process)



Most part of the Mg leached from the ore remained in the tailings water



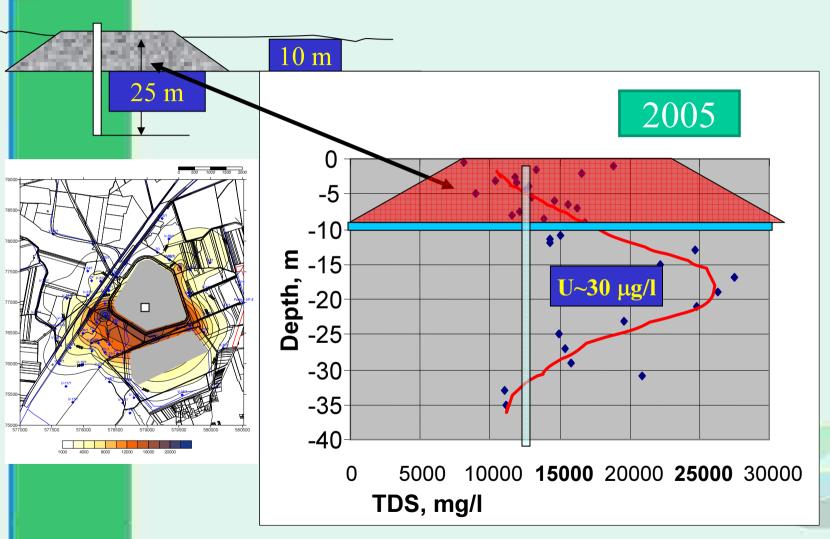
The distribution of the total cost between the sub-projects



Planned cost of remediation (1997-2002): 18,5 Billion HUF (74 Million EU)

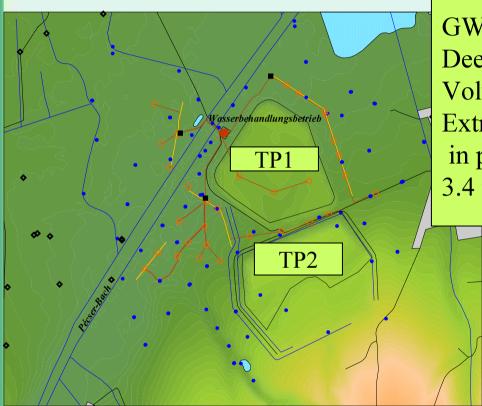


3.4.1 CONTAMINATION UNDER THE TPS





MEGSEK-ÖKO 3.3.3 GROUNDWATER RESTORATION



GW extraction wells: 27
Deep dranage: 3.2 km
Volume of the extracted
Extracted volume of water
in period of (2001-2008) was
3.4 million m³, 44 kt of TDS.



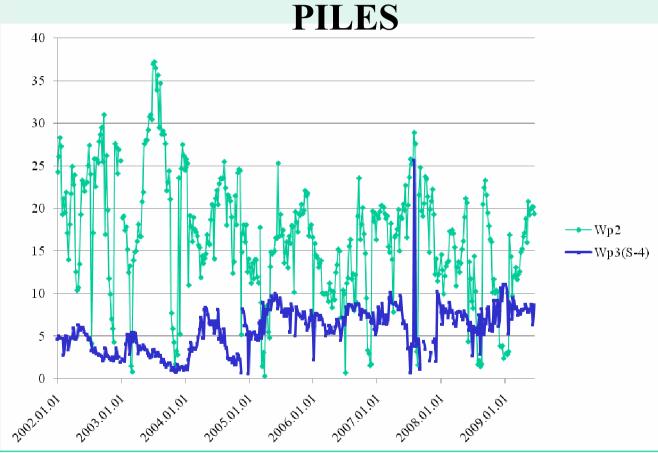
Yearly operation cost: 800 000 US \$ (~1.9 US \$/m³)

Water treatment: pump and treat with lime milk.

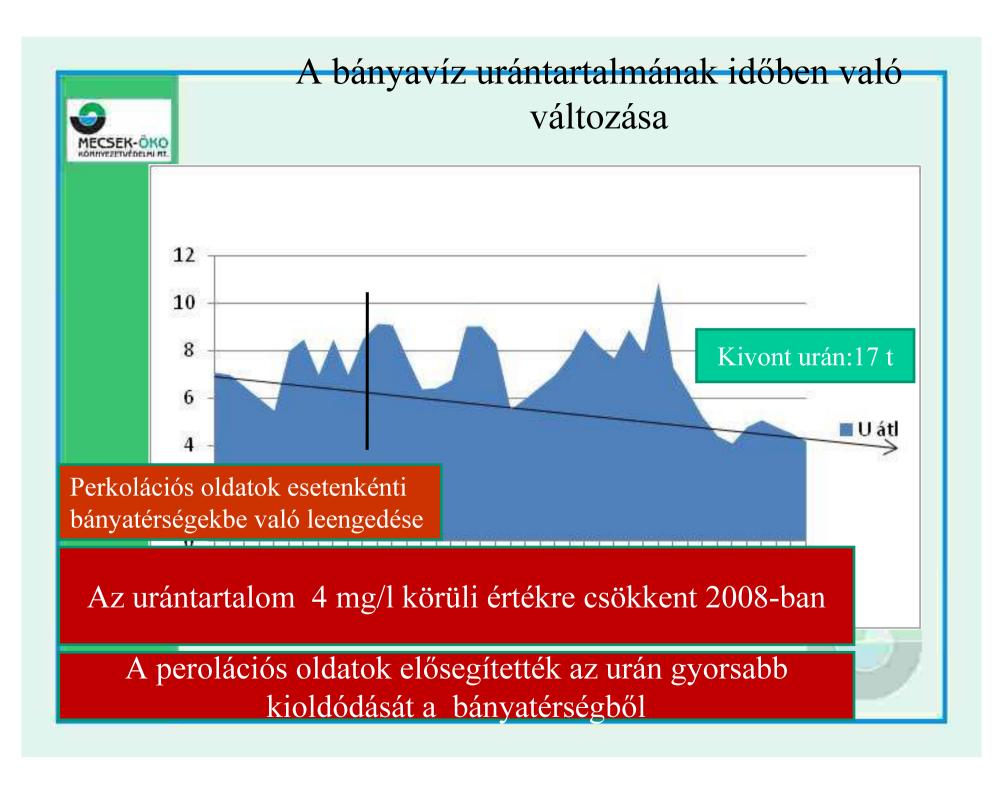
Sludge: Dry 3-4 kt/a)



3.1.1 URANIUM IN THE SEEPAGE OF WASTE ROCK

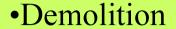


It can be expected that the uranium attenuation will be slow process





REMEDIATION OF THE MILL SITE



•Clean-up with soil replacing (0.35 Million m³)

The most contaminated ground was found on the ore and acid storage site, as well as under the yellow cake production facilities.

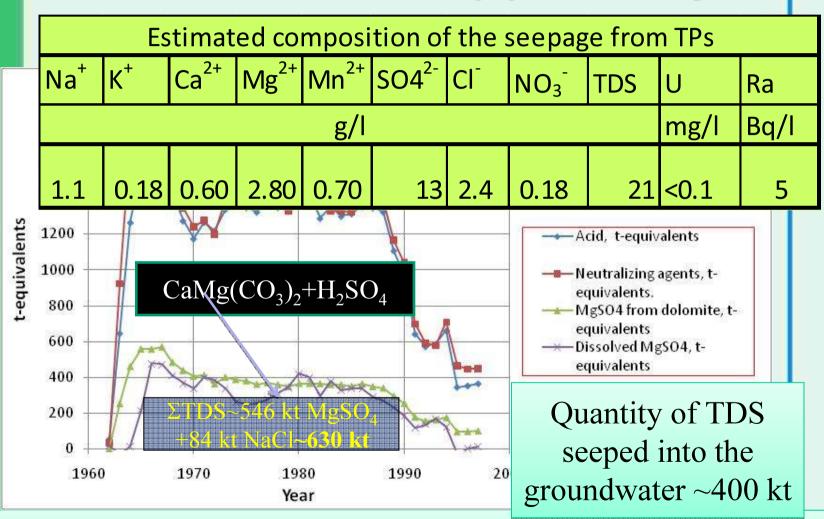
Scraps of mill balls

Total cost of remediation of the mill site:~ 5 million US \$; ~0.37 US \$/kgU



Assasement of the quantity of dissolved compounds disposed on tailings ponds

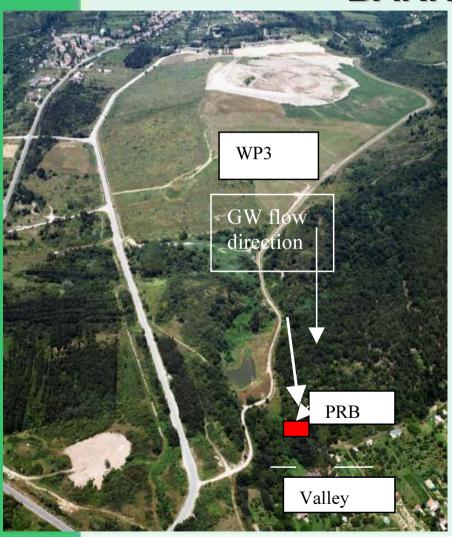
(Balance of acid and neutralizing agents in the mill process)



Most part of the Mg leached from the ore remained in the tailings water



PERMEABLE REACTIVE BARRIER



The installation is located in a narrow valley at the foot of WPN3, linking the mining area with drinking water aquifer (Zsid-valley)



LONG-TERM PERFORMANCE OF THE INSTALLED EXPERIMENTAL PRB

