Ivanov V., Skupov M., Shadrin A.

Closed nuclear fuel cycle with fast reactors and dense fuel

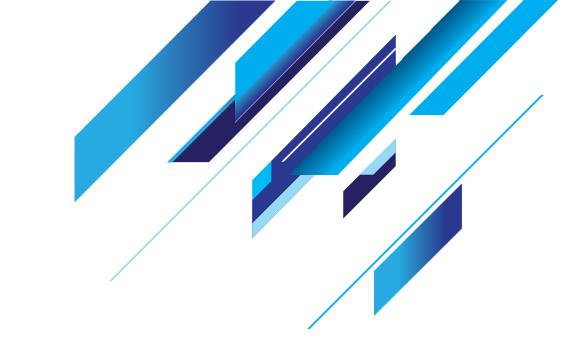
Shadrin A., Dvoeglazov K., Ivanov V.

Reprocessing of spent mixed nitride U-Pu fuel

from BREST-OD-300 reactor



ROSATOM goal in the back-and is a closed nuclear fuel cycle



3СЖЦ back-end



Очень велик too long



Что делать с хвостом?what to do with the back-end?

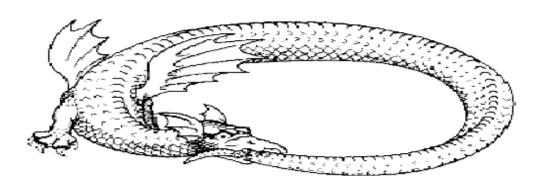


Отбросить? to fall off?



Сделать так, чтобы хвост не рос to prevent SNF accumulation





Утилизировать наследие to utilize the nuclear heritage



Вот, собственно, зачем мы создаем ту самую систему обращения с ОЯТ that's why we dovelon the system of SNE

that's why we develop the system of SNF management

Closed NFC whit Pu fuel

SNF accumulation

Cost of SNF storage (100 year) - around 200 - 400 USD for per kg

Recovered Pu storage – around 1 - 5 USD for 1 g per year or – 100 - 500 USD for 1 g per 100 years

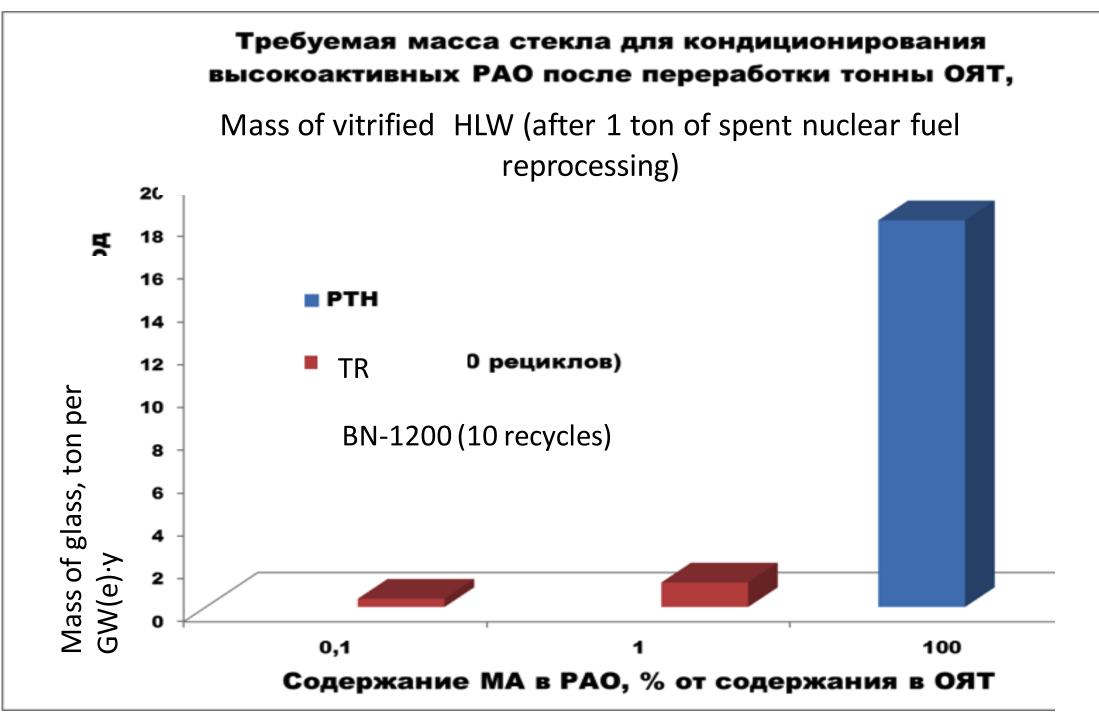
1 kg of terman reactor SNF contains several g of Pu

Main aim of Closed NFC is decrease of full expenses on SNF and Pu storage and radwaste treatment using Pu and MA as a fuel

Options for closed NFC whit Pu fuel:

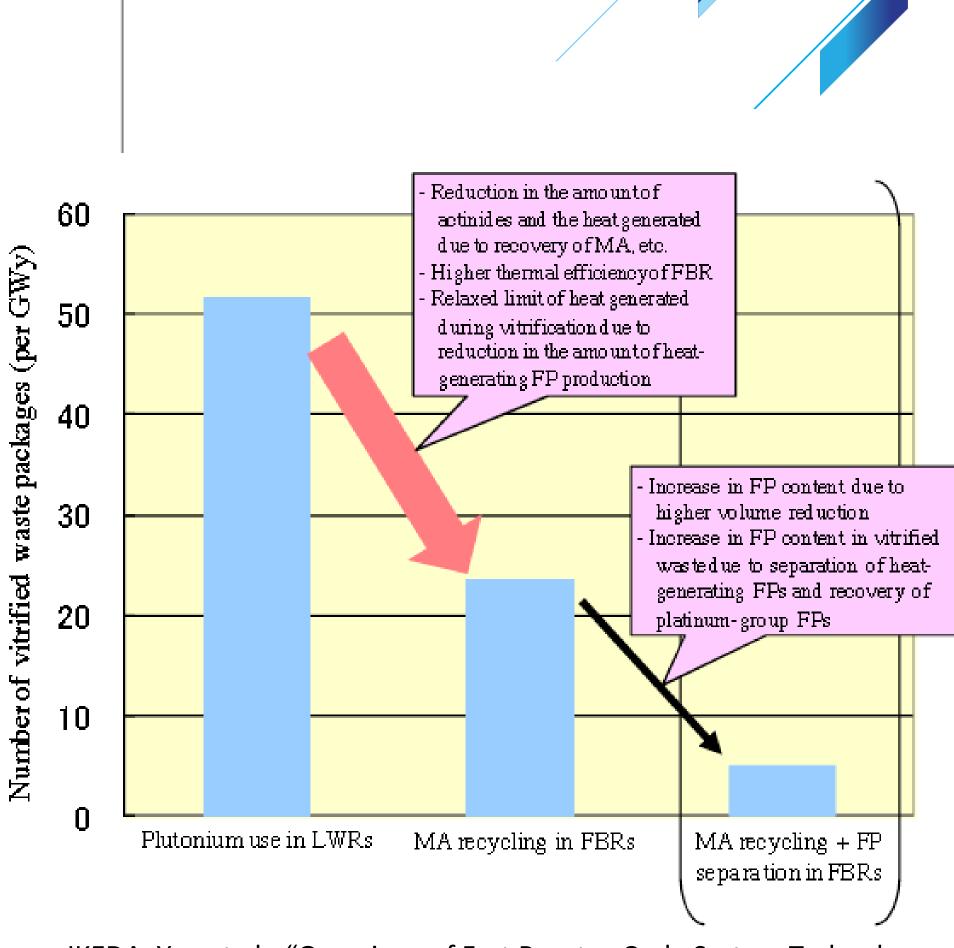
- REMIX
- MOX for thermal reactors
- MOX for fast reactor
- MNIT for fast reactor

Way we need partitioning



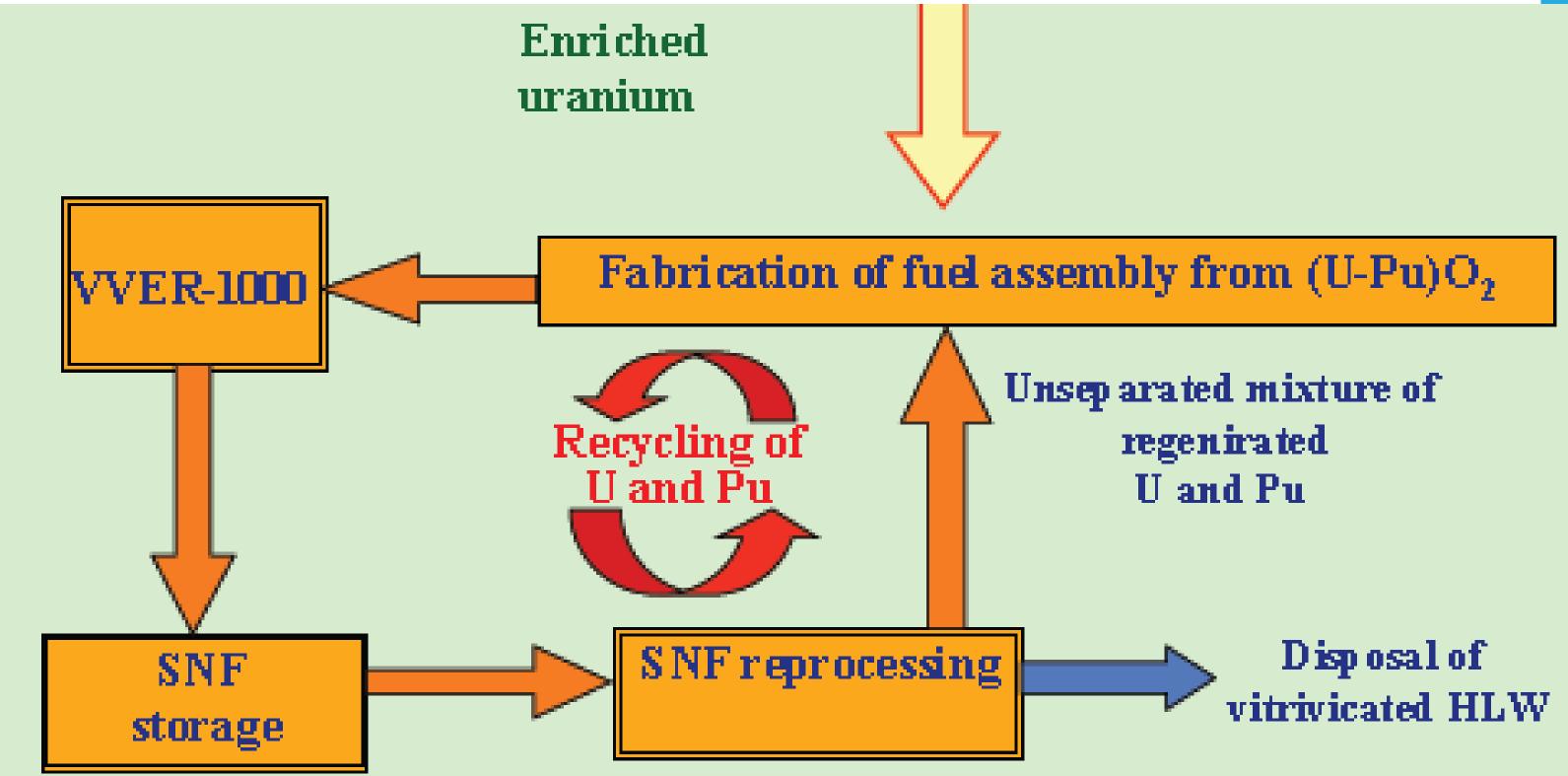
MA content in HLW, % of content in SNF

Volume of wastes containing MA for recycling in BR is negligibly small as compared with that from TR SNF reprocessing



IKEDA, Yo., et al., "Overview of Fast Reactor Cycle System Technology Development Project (Fact) Phase 1 and Future Direction", Global 2011 (Proc. Int. Conf., Makuhari, Japan, 2011), paper # 451660.

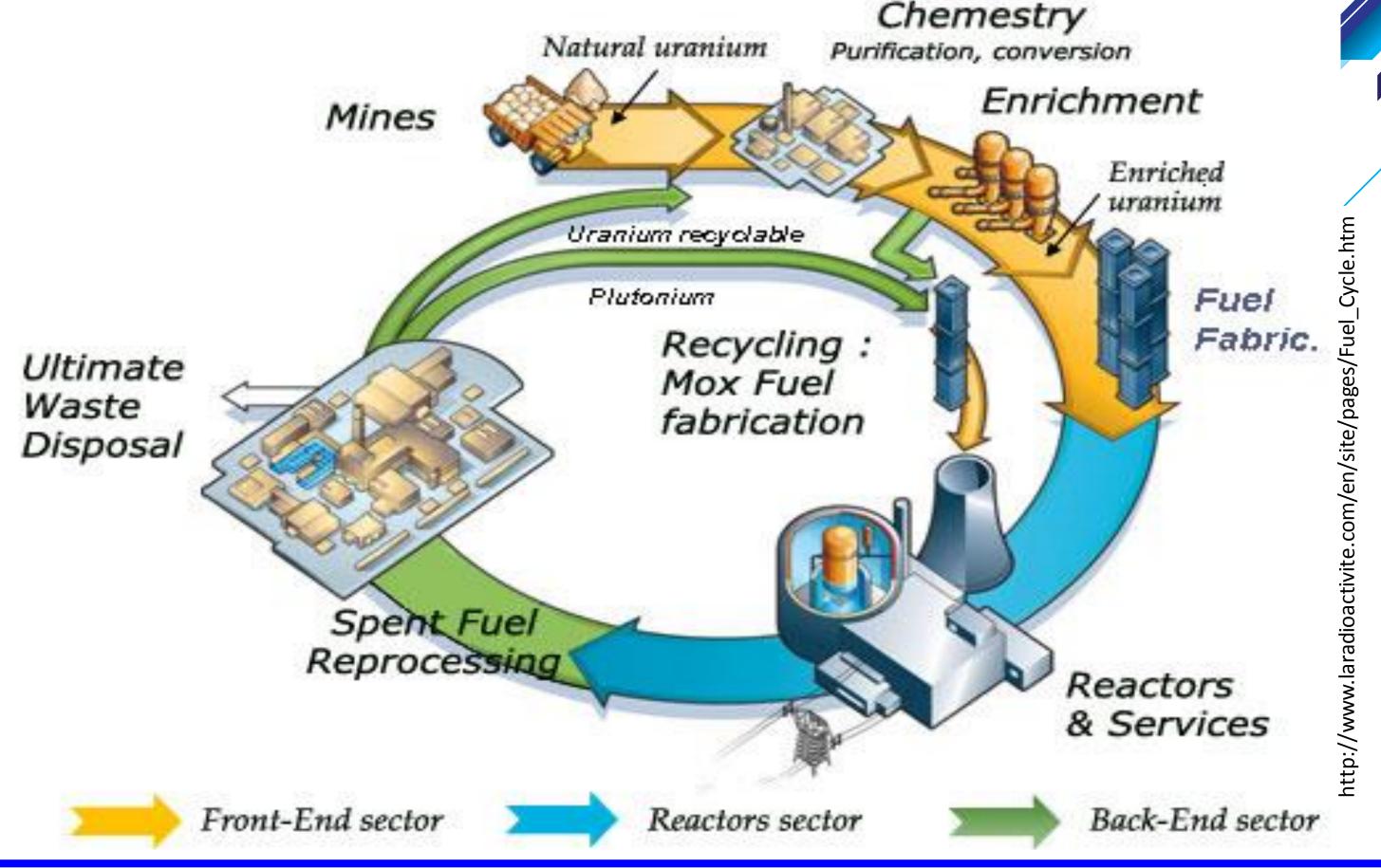
REMIX



Безопасность Окружающей Среды Nº1-2010: Обращение с ОЯТ

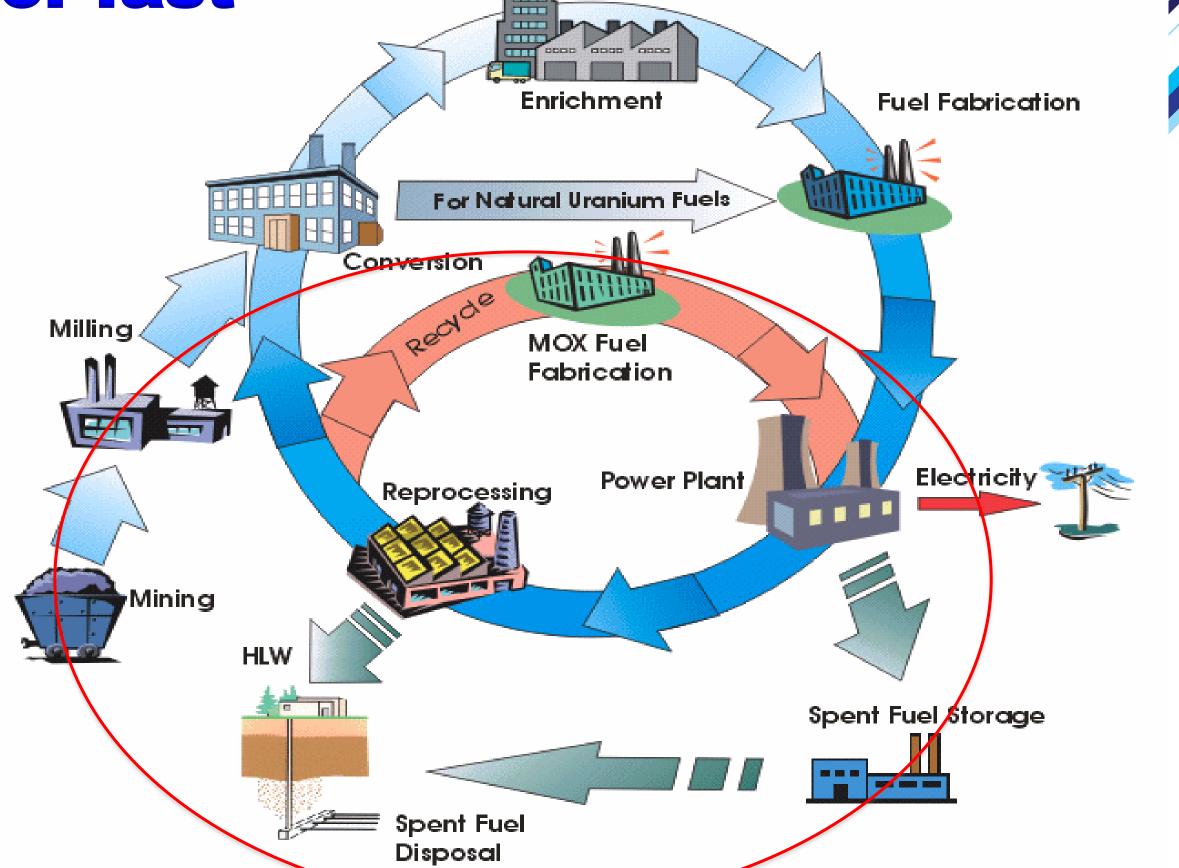
- U and Pu are involved in NFC
- Np, Am, Cm are in HLW jointly with fission products
- 6 times recycle of U and Pu

MOX for thermal reactors



- U and Pu are involved in NFC
- Np, Am, Cm are in HLW jointly with fission products
- 1 or 2 times recycle of U and Pu

MOX and MNIT for fast reactors

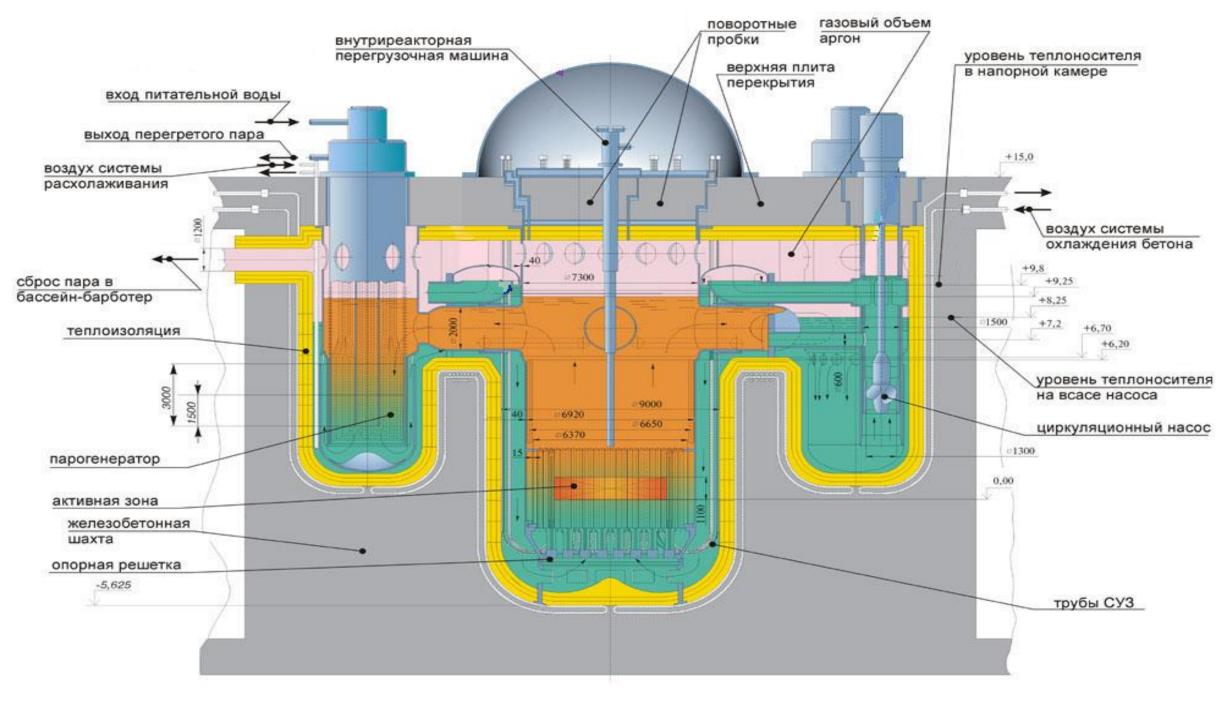


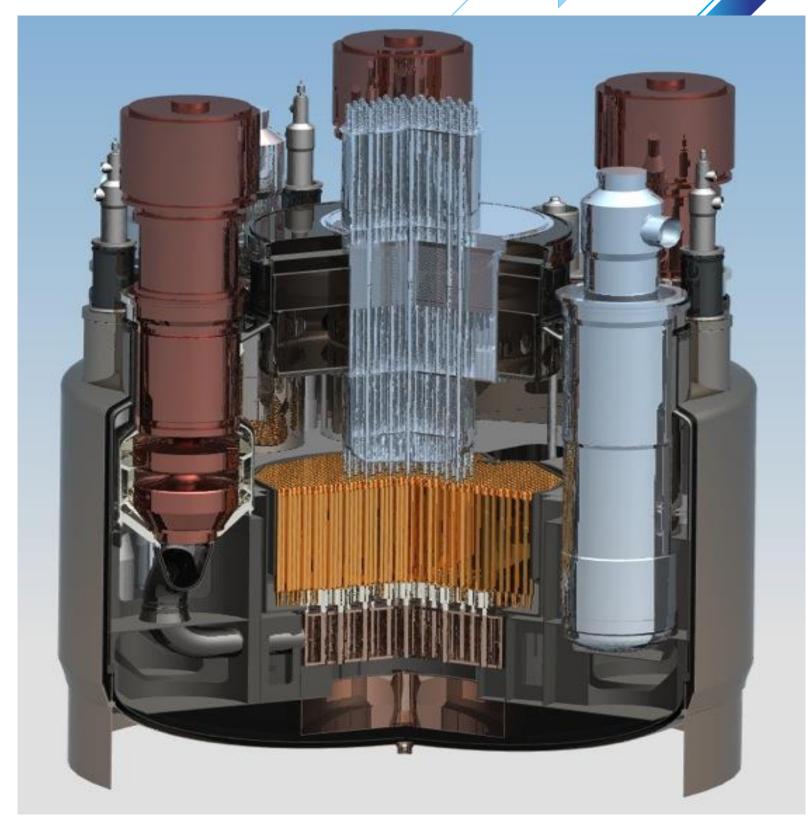
- U and Pu are involved in NFC and Np and Am will be involved
- Cm will be stored for long time and could be involved in NFC
- No limitation recycle of U and Pu

High capacity fast reactors

BREST-1200

BN-1200





Coolant – Pb Fuel – MNIT (U-PuN)

Coolant – Na Fuel – MNIT (U-PuN) MOX (U-PuO₂)

MOX or dense fuel?

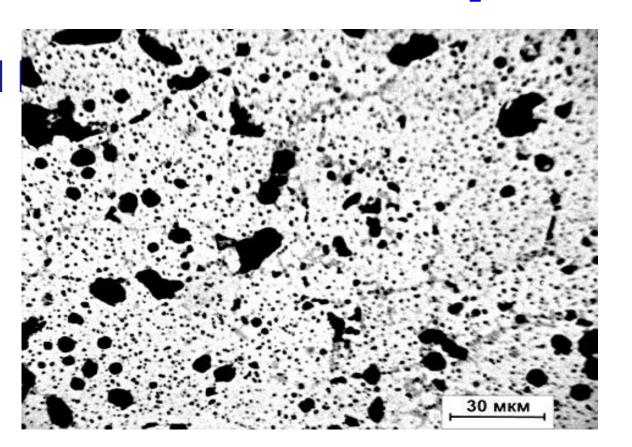
- Main questions
- Safety level
- Pu reproduction in active core
- Pu reproduction coefficient ~1.05
 without blanket
- 0.5% **ΔK/K** during all company
- Compatibility of MNIT is shells material
- Compatibility of MNIT with Na and coolant

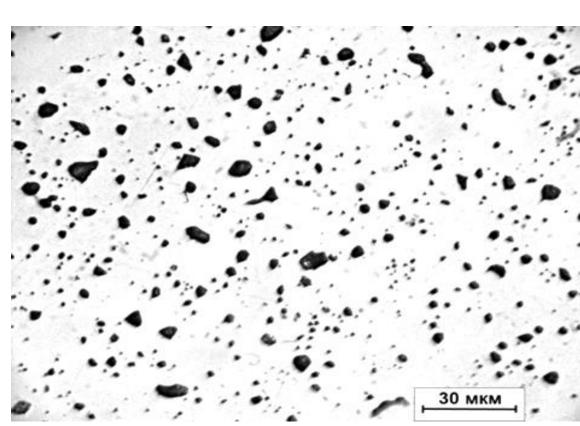
 $500 \, \mu m$

Experience of use U nitride fuel

Answer – dense fuel (metal, carbide, nitride) is better an compare with MOX.

However – MOX fabrication and MOX UNF reprocessing are industrial process





а в Микроструктура (U,Pu)N топлива с

выгоранием - 5 % т.а. (а) и 4 % т.а. (b)

MOX and MNIT for fast reactor today in Russia









- U and Pu are involved in NFC and Np and Am will be involved
- Cm will be stored for long time and could be involved in NFC
- No limitation recycle of U and Pu

Basic requirements for FR SNF reprocessing technologies

Imperative

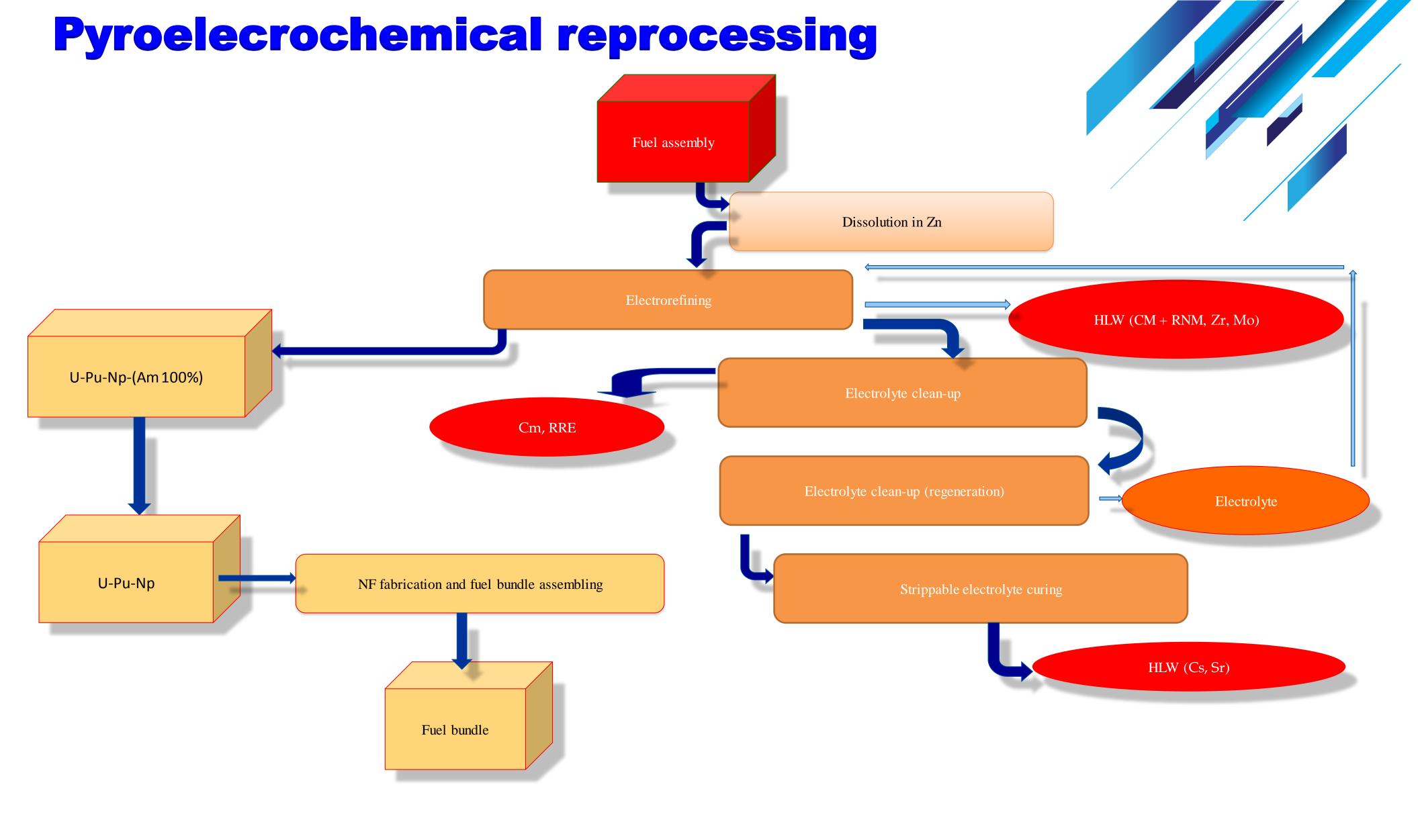
- 1. Safety
- 2. Ecological acceptance
- 3. Economic efficiency

Technical

- 1. Ability to reprocess SNF with low cooling time and high burnup
- 2. Observance of Non-Proliferation Treaty
- 3. Pu loss less than 0,1 %
- 4. End products suitable for fuel fabrication
- 5. Low volume of high-level waste
- 6. Partitioning

On-site reprocessing

Cooling time	1 year
Recycle of fissile	
materials	99,9 %
	Mixed U-Pu nitride
Type of SNF	or
	MOX
Separation U, Pu,	
Np	Not provided
U-Pu-Np	
purification	Up to 10 ⁶ from 10 ³
coefficient	
Transmutation of	Homogeneously or
minor actinides	heterogeniously



PH-process is a combine technology for FR SNF reprocessing Irradiated fuel Dissolving in liquid assemblies zinc **For storage** HLW (CM + RNM, Zr, Mo) Electrorefining **Pyro** Electrolyte U, Pu, Np Electrolyte cleaning Am (10%) Affinage (Fissionable materials **Hydro** extraction) Fissionable materials **Radwaste** REE and TPE group Am and Cm Am, Cm, REE Electrolyte cleaning U, Pu, Np separation separation (Am, Cm, REE removal) Am Oxides Electrolyte cleaning Cm, REE production (Regeneration) NF fabrication Oxides production. Output electrolyte and fuel bundle Storage solidification Fuel assemblies assembling To the storage HLW (Cs, Sr) Mid-level waste High-level waste treatment treatment **HLW** For storage

Combine technology (PH-process) is a palliative solution



However, PH-process:

- allows to reprocess SNF with low cooling time and high burn-up
- meets requirements of non-proliferation treaty
- allows to re-use > 99,9 % of fusible materials
- allows to produce mixed U-Pu-Np product of any purification grade
- Include Am and Cm recovery and separation

PH-process shold meets requirements:

- Safety
- Ecological acceptance
- Economic efficiency

Schedule for reprocessing facility (module)

(RM) of pilot and demonstration

energy complex (PDEC)

Pilot scale experiments

"Cold", "warm" and "hot" experiments at RIAR, PA "Mayak", Siberian Chemical Combine, Bochvar Institute
(HYDRO)

"Cold" experiments at RIAR (PYRO)



Combine test of technology

Equipment manufacturing

MR Design

RM construction

Start of operation and tests

2014 2015 2016 2017 2018 2019 2020 2021 2022



Technology and equipment

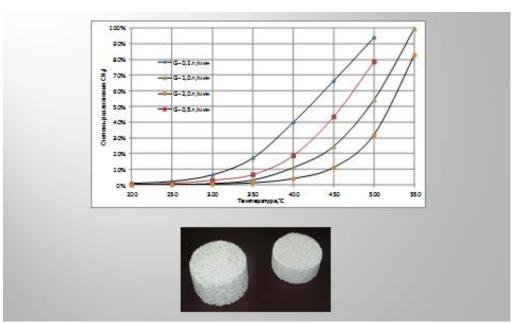
Up today following operation have been tested with simulated in irradiated fuel in lab scale:

- Shell removal
- Distillation of Zn/Cd/salt
- Pyroelectrorefining of MNIT
- Off gas treatment
- Salt purification and recycling

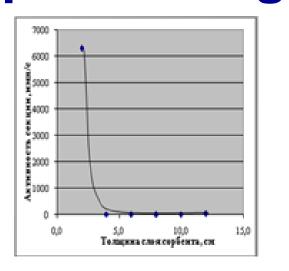
Experimental equipment for off gas treatment

Tests of pilot equipment and study of process conditions using full scale simulant MNIT SNF 2016-2018

Tests with irradiated MNIT would be done on EDEC reprocessing facility



Removal of CH₃I



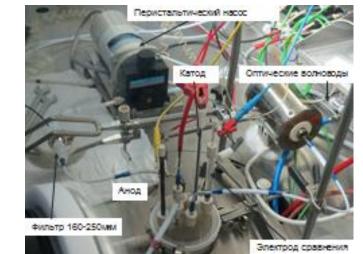
Removal of I₂



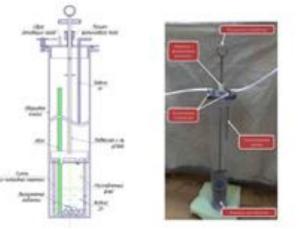
Experimental equipment for salt crystallization purification

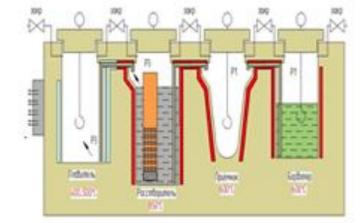






Tests of permanent pumping of liquid metal (Gas-In) and salt (LiCl-KCI-CsCI-NdCl₃ 330 °C, 200 hours





Experimental equipment for shell removal.

Zn after tests



Equipment design

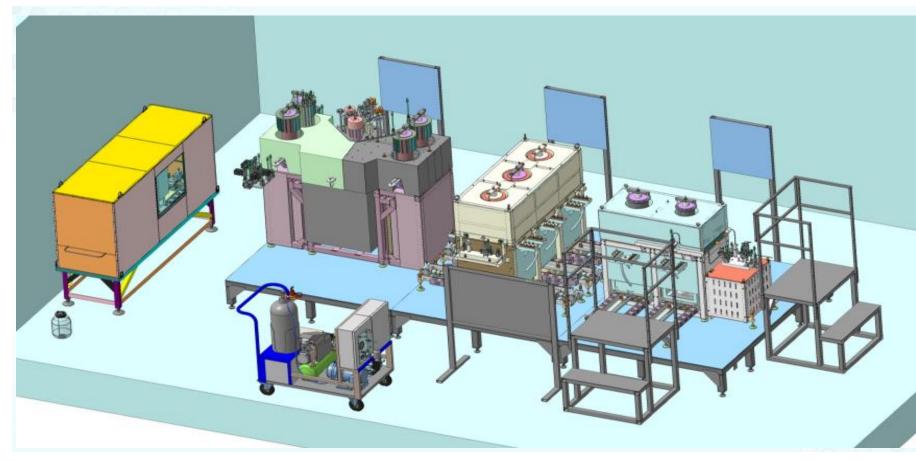
Experimental equipment



Design of industrial equipment should be completed in 2015



Argon cell should be put in operation in end of 2015



HYDRO Main results up today

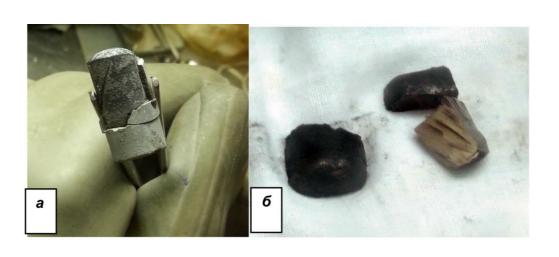
Tested with simulated and irradiated fuel:

- Dissolution of U-Pu-Np ingot
- Flow (membrane) clarification
- Partitioning
- Preparation of actinide oxides
- Intermediate and high level radwaste



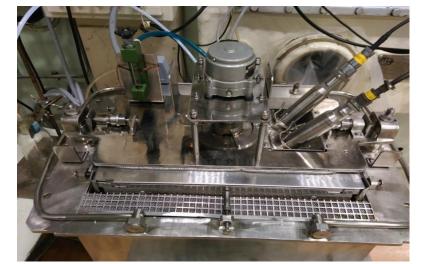
Desruction of NH₄NO₃ during distillation

2015-2018 task is to test all operation using pilot scale (prototype) equipment



a – ingot U-Pu-Npδ – ingot U-Pu-Npseparated in 3 parts





Oxide of actinides





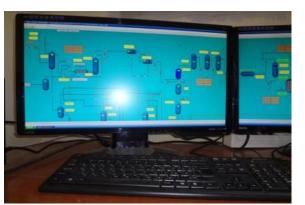
HYDRO

Laboratory and pilot mock-up for hydrometallurgy

Laboratory and hot cell set-ups







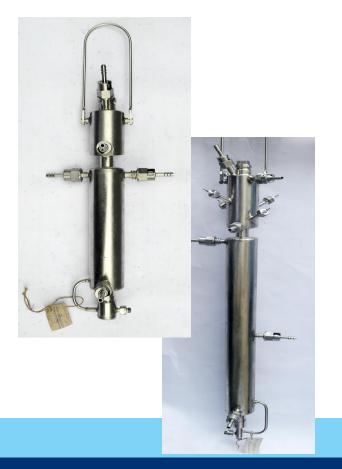






High temperature treatment including oxidation











Initial task – there is no the industrial technology for treatment of radwaste from BREST-300-OD MNIT SFF reprocessing

Reasons:

- Low time of SNF cooling;
- Loses of fissile materials with radwaste < 0,1%;

Solution – use of compact equipment with low capacity

Important – all technical solutions should not increases the time needed for achievement of radioecology equivalency

Radwaste Main results up today

- Principal design of equipment
- Crystallization and glass verification were selected as basic methods
- Principal design of container for all kind of filters, including HLW filters for liquid metals and melted salt







Tasks 2015-2017:

- Test of full-scale crystallization set-up
- Test of full-scale cold crucible
- R&D for basis of process safety

Computer codes for nuclear fuel cycle technologies and objects development

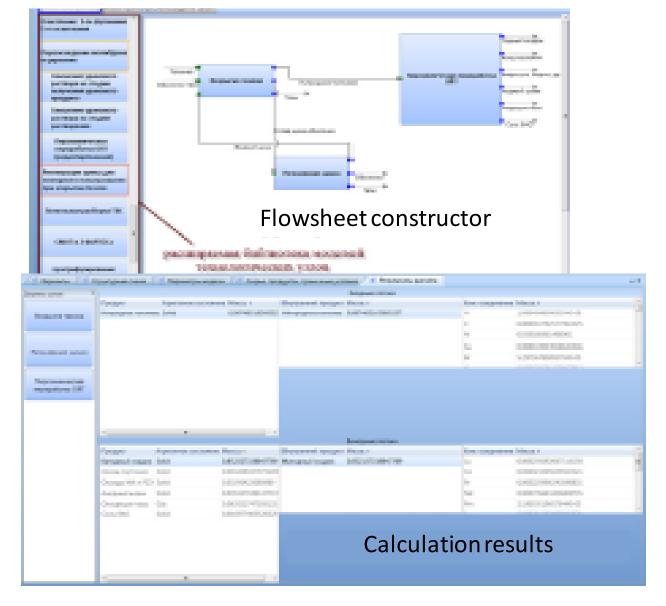




BALANCE MODELS OF INF REPROCESSING, NUCLEAR FUEL FABRICATION/REFABRICATION AND RADIOACTIVE WASTE TREATMENT

Objectives:

Evaluation feasibility of technological solutions while developing flow sheet; balance calculations of material flows and generated waste; flow sheets optimization



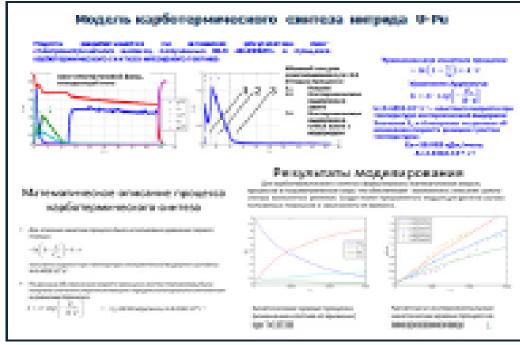
This mathematical tool significantly decreases time and resources required for calculations and comparison of multiple flow sheet options



Objectives:

Calculation and optimization of processes operation modes, substantiation design decisions, emergency modes description

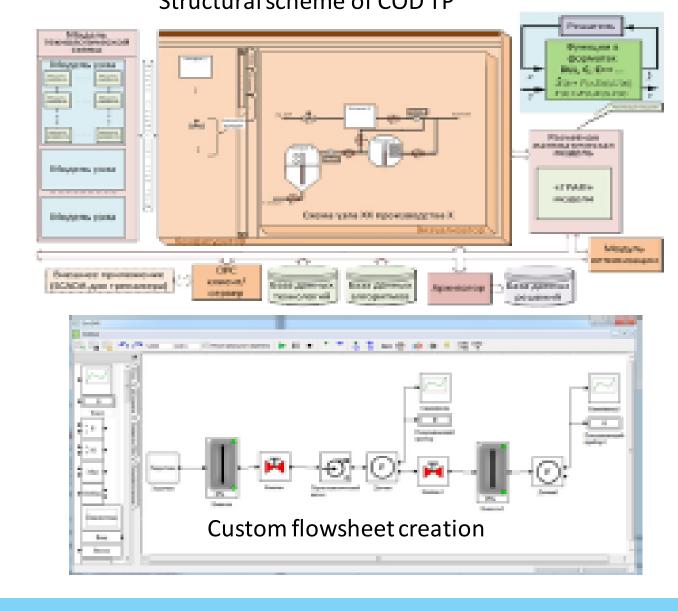




COMPUTER CODE FOR OPTIMIZATION AND DIAGNOSTICS OF TECHNOLOGICAL PROCESSES (COD TP)

Objectives:

Simulation of On-Site NFC flow sheet operation for investigation of operability and controllability and optimization as separate processes, technological nodes and setups, so the whole On-Site NFC flow sheet. Also the COD TP is purposed for simulation of control and operation of the whole flow sheet or separate elements with further usage of the simulation results for creating real ADCC



Conclusion (1)

There are several options for closed NFC whit Pu fuel:

- REMIX
- MOX for thermal reactors
- MOX for fast reactor
- MNIT for fast reactor

The high density fuel is the only type of nuclear fuel which is able to provide CNFC realization.

CNFC with MNIT and PH-process allows:

- reprocessing of FBR SNF with high burn up and low cooling time;
- decrease the volume and time of SNF storage
- •to reprocess any type of SNF;
- •to prepare the final uranium neptunium plutonium product running the requirements for fabrication of the final pelleted mixed (U,Pu)N fuel.

Conclusion (2)

- By now following basic technological operations have been tested in laboratory conditions on real products:
 - steel cladding removal by dissolution in molten Zn;
 - pyroelectrochemical recovery of U, Pu and Np;
 - extraction refining of U, Pu and Np;
 - separation of rare earth elements and transplutonium elements.
- Experimental set-ups to test engineering solutions for pyroelectrochemical equipment should be installed in argon cell in 2015
- The installation for test of innovative systems for hydrometallurgical operations was completed 2014
- Design of MNIT SNF reprocessing and waste treatment unit was started in 2015

Conclusion (3)

At present time design of the pilot demonstration power complex (Seversk, Siberian Chemical Combine) for fuel fast reactor fabrication and FR SNF reprocessing is started.

The complex includes

- •reactor
- fabrication and refabrication facility
- reprocessing of SNF and waste treatment facility.

Operation start:

- Fuel fabrication 2018
- Reprocessing of SNF and waste treatment 2021
- Refabrication of MNIT fuel 2024.